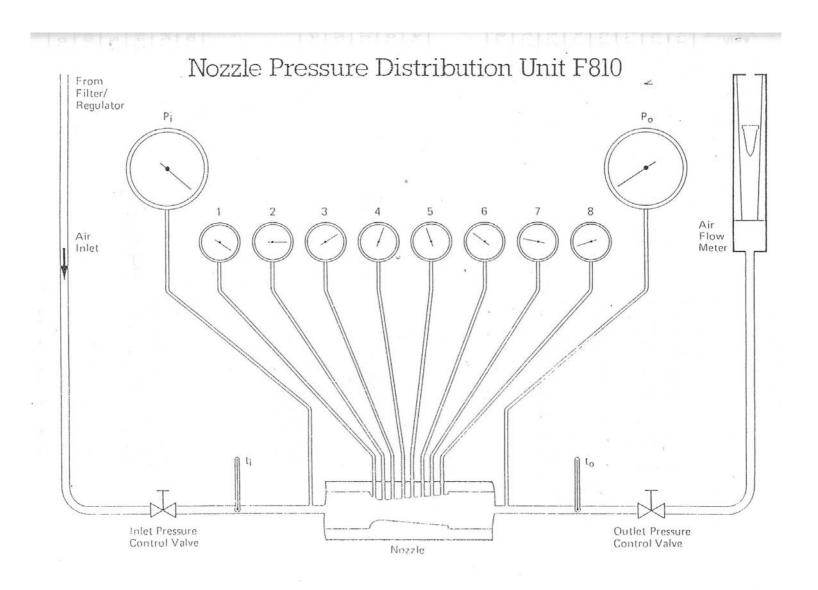
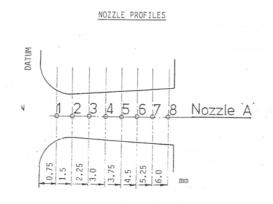
Nozzle pressure measurements

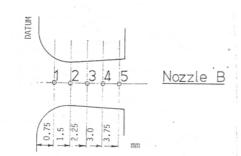
- The objectives are to measure the flow rates and pressure distributions within the converging and diverging nozzle under different exit and inlet pressure ratios.
- Analytic results will be used to contrast the measurements for the pressure and normal shock locations.

equipment setup



Nozzle types





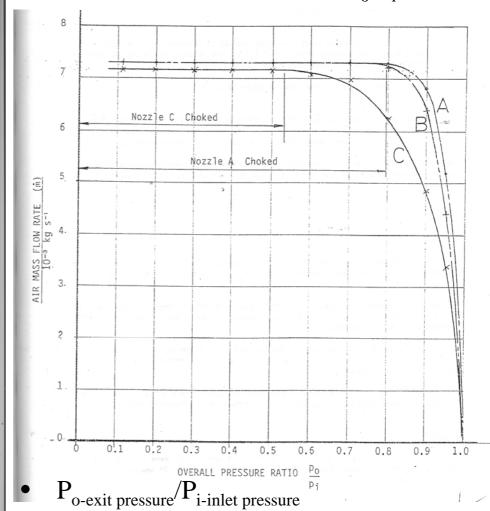
			-			DATUM		
		1	2	3	4	5 6	Nozzle	C
/	-	6.25	5.25	4.25	3.25	1.25	mm	

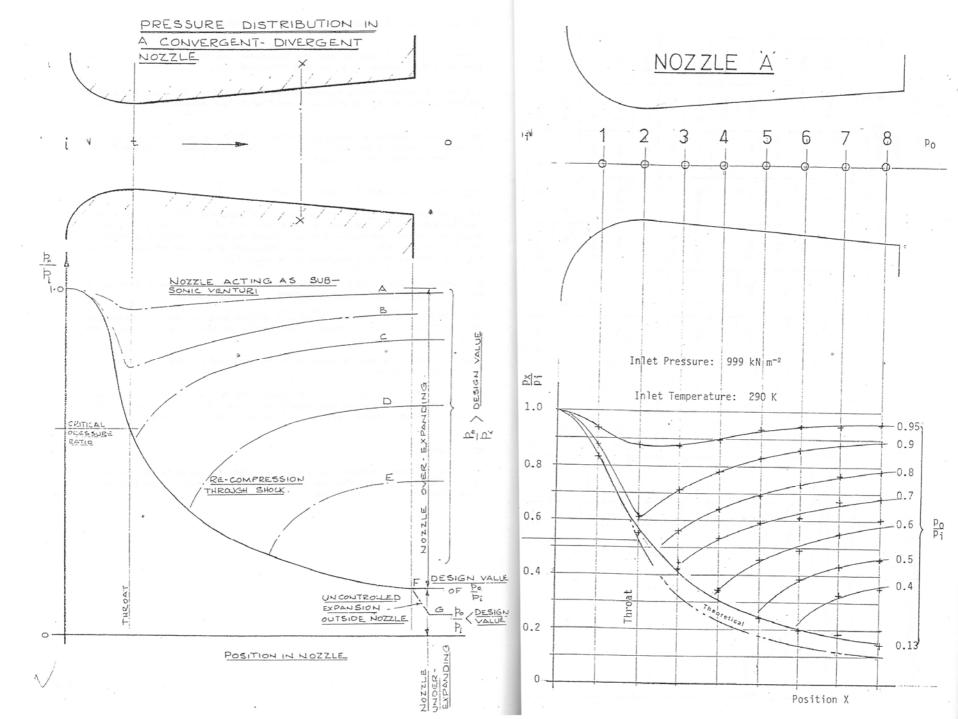
		- 20	
Tapping Point	Nominal Diameter mm	Area Throat Area	
1	2.4	1.44	
2	2.0	1.0	
3	2.13	1.13	
- 4	2.26	1.28	
5	2.39	1.42	
6	2.52	1.59	
7	2.66	1.77	
8	2.79	1.94	

1	2.4	1.44
2	2.0	1.0
3	2.13	1.13
4	2.26	1.28
5	2.39	1.42

1	2.86	2.05
2	2.65	1.75
3	2.43	1.48
4	2.21	1.2
5	2.03	1.03
6	2.0	1.0

• Mass flow rate at different P_o/P_i



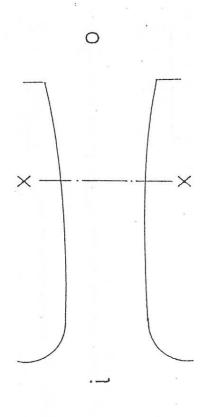


Final report

- Introduction
- Theory
- Experimental setup
- Measured and theoretical results
- Discussion
- Conclusion

THEORY

Flow through a nozzle



For reversible and adiabatic one dimensional expansion through a passage, the following relationships apply at any section XX.

$$C_{x} = \sqrt{2(h_{1} - h_{x})}$$

B

11 If it is assumed that the relationship between p and v in such an expansion is pv^k constant,

$$h_{i} - h_{x} = \sum_{i}^{x} vdp$$

$$= \frac{k}{k-1} p_{i}v_{i} \begin{bmatrix} 1 - (\frac{p_{x}}{p_{i}})^{k} - 1 \\ p_{i} \end{bmatrix}$$

and substituting this in A,

$$C_{x} = \sqrt{\frac{2k}{k-1}} p_{i}v_{i} \left[1 - \frac{p_{x}}{p_{i}} \frac{k-1}{k} \right]$$

0

U

$$v_{X} = \frac{(P_{1})}{(P_{X})} \frac{1}{K}$$

and, substituting for C_{χ} and v_{χ} in B,

$$A_{x} = \frac{\frac{p_{i}}{m} \frac{1}{k^{x}}}{\frac{2k}{k-1} p_{i} v_{i}} \frac{1}{1 - \binom{p_{x}}{k}} \frac{k-1}{k}$$

Rearranging,

$$\frac{\dot{n}}{A_{x}} = \sqrt{\frac{2k}{k-1}} \frac{p_{1}}{v_{1}} \left[\frac{(p_{x})}{p_{1}} \frac{\frac{2}{k}}{k-\frac{(p_{x})}{p_{1}}} \frac{\frac{k+1}{k+1}}{p_{1}} \right]$$

ш

This expression has a maximum value, when

$$\frac{p_x}{p_1} = (\frac{2}{k+1})^{\frac{k}{k-1}}$$
 (This is called the Critical Pressure Ratio)

the at. i.e. smallest value, its has a maximum when $A_{\rm X}$ ı.s AX · E i is a constant, "throat". Sincle

Thus,
$$\frac{p_{t}}{p_{1}} = (\frac{2}{k+1}) \frac{k}{k-1}$$

L

If this value is substituted in D,

$$C_t = \sqrt{\frac{2k}{k+1}} P_1 v_1$$

C

which is the local speed of sound. = 4 k ptvt ť

Or

... e into equation B, Substituting the throat conditions

and
$$c_t = \sqrt{\frac{2}{k+1}} \, \stackrel{\text{piv}_i}{\text{pi}_i}$$
 and
$$v_t = (\frac{2}{k+1}) \, \frac{-1}{k-1} \, \stackrel{\text{v}_i}{\text{v}_i}$$
 we obtain
$$\frac{\hat{m}}{A_t} = (\frac{2}{k+1}) \, \frac{1}{k-1} \, \sqrt{\frac{2k}{k+1}} \, \frac{p_i}{v_i}$$

I

the area and If Equation H is divided by E we obtain the relationship between the throat section x. area at any

$$\frac{A_{X}}{A_{L}} = \frac{2}{(k+1)} \frac{1}{k-1} \sqrt{\frac{k-1}{(k+1)} \left[\frac{P_{X}}{P_{1}} \frac{2}{k} - \frac{P_{X}}{P_{1}} \right]}$$

5

and for nozzle exit,

$$\frac{A_0}{A_{t}} = \frac{2}{(k+1)} \frac{1}{k-1} \left(\frac{1}{(k+1)} \left(\frac{P_0}{P_1} \right) \frac{2}{k} - \frac{P_0}{P_1} \right) \frac{1}{k} \right)$$

×

and a compressible fluid expands reversibly adiabatically in a passage through a pressure ratio when be seen that From the foregoing it will

$$\frac{P_0}{P_1} < (\frac{2}{k+1})^{\frac{K}{k}}$$

The passage must have reducing cross-sectional area, i.e. converge, until (i)

$$\frac{p_t}{p_j} = (\frac{2}{k+1})^{\frac{k}{k-1}}$$

and must then have increasing cross-sectional area, i.e. diverge.

-

- At the minimum area in the passage, i.e. the throat, the velocity of the fluid is the local speed of sound. (ii)
- In the converging portion, velocity will be subsonic and in the diverging portion will be supersonic. ·(iii)
- The mass flow rate through the passage is determined by the cross-sectional area It is not affected by the value of p_2 as long as the critical pressure ratio is maintained at the throat of the throat and the properties of the fluid at inlet. (YI).

If the fluid flowing is a perfect gas we may use the following relationships:

 γ = Const, etc and during a reversible and adiabatic process p_{v}

perfect gas For air at the conditions met in this unit, we may assume that it behaves as

$$R = 287.1 \text{ J kg}^{-1} \text{ K}^{-1}$$

$$c_{\rm p} = 1005 \ {\rm J \ kg^{-1} \ K^{-1}}$$

Using these relationships, Equation C becomes

$$C_{x} = \sqrt{\frac{2\gamma}{\gamma-1}} RT_{1} \left[\frac{1}{1} - \left(\frac{p_{x}}{p_{1}}\right)^{\gamma} \frac{1}{\gamma} \right]$$

$$= \int \frac{2 \times 1.4 \times 287.1}{0.4} \int T_{i} \left[1 - \left(\frac{P_{X}}{P_{i}} \right) \frac{0.4}{1.4} \right]$$

= 44.83
$$I_1 \left[1 - \left(\frac{p_X}{p_1} \right) 0.286 \right] \text{ m s}^{-1}$$

۲

Equation H becomes

$$\dot{m} = A_{t} \left(\frac{2}{\gamma + 1}\right)^{\frac{1}{\gamma - 1}} \sqrt{\frac{2\gamma}{\gamma + 1}} \frac{P_{i}^{\frac{2}{\gamma}}}{RT_{1}}$$

$$= A_{t} \left(\frac{2}{2 \cdot 4}\right)^{\frac{1}{0 \cdot 4}} \sqrt{\frac{2 \times 1 \cdot 4}{2 \cdot 4 \times 287 \cdot 1}} \frac{P_{i}}{T_{i}}$$

$$\dot{m} = 0.0404 \sqrt{\frac{A_{t}P_{i}}{T_{i}}} \text{ kg s}^{-1}$$

Equation G becomes

$$C_{t} = \sqrt{\frac{2\gamma}{\gamma + 1}} RT_{i}$$

$$= \sqrt{\frac{2 \times 1.4 \times 287.1 \times T_{i}}{2.4}}$$

$$C_{t} = 18.3 \sqrt{T_{i}} m s^{-1}$$

It should be appreciated that the above relationships apply to reversible and adiabatic, i.e. isentropic, flow.

Although flow through practical nozzles may usually be assumed to be adiabatic, there will be various losses due to friction and shock — particularly in the divergent portion — which will render the expansion irreversible.